CITIA GORG GNIVERZITET CRNE GORE MAGDALURŠKO-TFHNOLOŠKI FAKULTE T

Metalurško tehnološki fakultet

Vijeću

8roj 7237 71. 10 20 god.

Predmet: Saglasnost za nastavak procedure za MSc Zoranu Sekulić, studentkinju doktorskih studija

U skladu sa članom 31a, **Pravila o izmjenama i dopunama pravila doktorskih studija (Bilten UCG br.561, od 4.07.2022)**, mentorka prof. dr Vanja Asanović je Komisiji za doktorske studije MTF-a, podnijela izvještaj o radu studentkinje doktorskih studija MSc Zorane Sekulić, a koji se odnosi na sprovedena istraživanja i postignute rezultate u studijskoj 2022/23. godini.

Komisija je izvršila uvid u obrazloženje mentorke o sprovedenim istraživanjima i publikovanim radovima u protekloj studijskoj godini. Konstatovano je da doktorandkinja ima 2 rada u časopisima sa SCI/SCIE liste, od kojih je jedan publikovan, a drugi prihvaćen za publikovanje i dostupan on line.

Rezutati koje je doktorandkinja postigla u prethodnoj studijskoj godini, detaljno su objašnjeni od strane mentorke, na osnovu čega je konstatovano da je doktorandkinja ostvarila napredak prema predvidjenom planu rada na tezi.

Na osnovu uvida u priložene radove i ocjene mentorke da kandidatkinja može nastaviti sa radom na istraživanjima, Komisija smatra da je doktorandkinja uspješno završila prethodnu studijsku godinu i predlaže nastavak daljih istraživanja u skladu sa istraživačkim planom.

Podgorica, Oktobra 2023

Komisiji

Prof. dr Mira Vukčević 3. Jeua Prof. dr Zorica Leka

Prof. dr Ivana Bošković

Crna Gora
UNIVERZITET CRNE GORE
METALURŠKO-TEHNOLOŠKI FAKLILTET

UNIVERZITET CRNE GORE Broj 220 god. METALURŠKO-TEHNOLOŠKI FAKULTET

Podgorica

PREDMET: Godišnji izvještaj mentora o napredovanju doktoranda

Poštovani,

U skladu sa Pravilima o izmjenama i dopunama pravila doktorskih studija (Bilten Univerziteta Crne Gore, br. 561 od 04.07.2022. godine), dostavljam Vam Godišnji izvještaj mentora o napredovanju doktoranda MSc Zorane Sekulić.

Srdačan pozdrav,

Mentor

Prof. dr Vanja Asanović

Podgorica, 09.10.2023.g.



UNIVERZITET CRNE GORE

ObrazacIM:Godišnji izvještaj mentora o napredovanju doktoranda

GODIŠNJI IZVJEŠTAJ MENTORA O NAPREDOVANJU DOKTORANDA

Akademska godina za koji	u se podnosi izvještaj	2022/202	23	·i.		
	OPŠTI PODACI O I	OKTOR	ANDU			
Titula, ime, ime roditelja, prezime	MSc Zorana Sekulić					
Fakultet	Metalurško-tehnološki f	akultet				
Studijski program	Metalurgija i materijali					
Broj indeksa	1/19					
	MENTOR/M	ENTORI				
Mentor	Prof. dr Vanja Asanović	UCG, Cr	na Gora	Fiz	ička meta	lurgija
Ko-mentor	Dr Jasmina Grbović Novaković	nauke "Vi Institut od	l og značaja za Srbiju,	1	ička hemi terijala	ija
	EVALUACIJA DO	KTORAN	IDA*			
Koliko ste zadovoljni kva sa doktorandom?	litetom održanih susreta		<u>2</u> [3	<u>4</u>	∑ 5
(Ako je prethodni odgovo	or "1" ili "2" dati obrazlož	enje i prije	dloge za po	boljša	nje)	
Da li je definisan plan rada			⊠DA]ne	
Da li je doktorand ost predviđenom planu rada?	tvario napredak prema		⊠DA]ne	
(Ako je prethodni odgovo		prijedloge	za poboljša	inje)		
Kvalitet napretka dokto rada u periodu za koji se p		1	<u>2</u> [3	<u>4</u>	⊠ 5
(Ako je prethodni odgovo	r "1" ili "2" dati obrazlož	enje i prije	dloge za po	boljša	nje)	
Ocjena doktorandove spre		<u></u> 1	<u>2</u> [3	<u>4</u>	∑ 5
Ocjena planiranja i istraživačkih aktivnosti i doktoranda.	<u></u> 1	<u> </u>	3	<u></u> 4	⊠ 5	
Ocjena napretka u sav naučno-istraživačkog rada		<u></u> 1	<u>2</u> [3	<u></u> 4	⊠ 5
Ocjena doktorandovog ge studijama.		<u> </u>	<u></u>	<u></u> 4	∑ 5	
Ocjena ukupnog kvaliteta	doktorandovog rada.	1	<u> </u>	3	<u></u> 4	∑ 5
(Ako je prethodni odgovo	r "1" ili "2" dati obrazlož	enje i prije	dloge za po	boljša	nje)	

 $^{^*}$ Ocjene su: 1 – nedovoljan, 2 – dovoljan, 3 – dobar, 4 – vrlo dobar, 5 – odličan

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ObrazacIM:Godišnji izvještaj mentora o napredovanju doktoranda

ISPUNJENOST USLOVA DOKTORANDA

Spisak radova doktoranda iz oblasti doktorskih studija koje je publikovao doktorand (dati spisak radova koji sadrži)

Doktorantkinja MSc Zorana Sekulić je rezultate sprovedenog istraživanja predstavila u sljedećim radovima koji su objavljeni u naučnim časopisima za sa SCI/SCIE liste:

- 1. Babić B., Prvulović M., Filipović N., Mravik Ž., Sekulić Z., Milošević Govedarović S., Milanović I., "Hydrogen storage properties of MgH₂—Tm: Ni-catalysis vs. mechanical milling", *International Journal of Hydrogen Energy*, 2023, SSN 0360-3199, Article in press, Available online 26 April 2023, https://doi.org/10.1016/j.ijhydene.2023.04.078. (https://www.sciencedirect.com/science/article/pii/S036031992301813X).
- **2. Sekulić Z.,** Grbović Novaković J., Babić B., Prvulović M., Milanović I., Novaković N., Rajnović D., Filipović N., Asanović V., "The Catalytic Effect of Vanadium on Sorption Properties of MgH₂-Based Nanocomposites Obtained Using Low Milling Time, *Materials*, 2023, 16, 5480. https://doi.org/10.3390/ma16155480.

Obrazloženje mentora o korišćenju sprovedenih istraživanja u publikovanim radovima (dati obrazloženje)

Planom istraživanja predviđeno je proučavanje faznih transformacija, ispitivanje strukture i kristalne strukture, istraživanje katalitičkog efekta 3d, 4d i 5d metala na sorpcionu kinetiku vodonika u nanokompozitnom materijalu, kao i uticaja na termodinamičku stabilnost magnezijum hidrida, MgH₂.

U radu Hydrogen storage properties of MgH₂-Tm: Ni-catalysis vs. mechanical milling", predstavljeni su rezultati istraživanja uticaja dodavanja nikla na desorpciju vodonika iz kompozita MgH₂-Ni. Kompozitni prah je mljeven 15 min, 30 min i 45 min, a za karakterizaciju kompozita su primijenjene: rendgenska difrakciona analiza (XRD), skenirajuća elektronska mikroskopija sa energetski disperzivnom spektrometrijom (SEM-EDS), laserska metoda za određivanje raspodjele veličine čestica (PSD), diferencijalna skenirajuća kalorimetrija (DSC) i temperaturno programirana desorpcija (TPD). Primijećeno je da ravnomjerna raspodjela utiče na snižavanje temperature desorpcije vodonika za više od 100 °C. Utvrđeno je da se reakcija desorpcije vodonika u katalizovanim uzorcima može opisati kinetičkim mehanizmom Avrami-Erofejeva (Avrami-Erofeev) sa vrijednošću parametra n = 4. Prividna energija aktivacije reakcije desorpcije vodonika se smanjivala sa povećanjem vremena mljevenja i dodatkom nikla. Ovo istraživanje je po prvi put pokazalo da se dva glavna procesa (mljevenje i katalitičko djelovanje) mogu zasebno analizirati. Zaključeno je da u toku kratkotrajnih vremena mljevenja, preovlađuje katalitički efekat nikla.

U radu The Catalytic Effect of Vanadium on Sorption Properties of MgH₂-Based Nanocomposites Obtained Using Low Milling Time, prikazani su rezultati analize uticaja katalitičkog efekta vanadijuma na desorpcione karakteristike kompozita. Primjenom mehanohemijskog mljevenja u visokoenergetskom kugličnom mlinu, kao metode zelene sinteze u inertnoj atmosferi argona, sintetizovan je kompozit magnezijum hidrid-vanadijum. Odnos mase kuglica i mase praha upotrijebljenog materijala BPR (Ball to Powder Ratio) iznosio je ≈ 10:1, a mljevenje magnezijum hidrida sa dodatkom vanadijuma u količini od 2 mas % i 5 mas % je realizovano pri različitim vremenskim intervalima od 15 min do 45 min. Mikrostrukturna istraživanja su sprovedena primjenom rendgenske difrakcione analize (XRD) i infracrvene spektroskopije sa Furijeovom



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transformacijom, morfologija je ispitivana pomoću skenirajuće elektronske mikroskopija (SEM), a utvrđena je i raspodjela čestica na osnovu njihove veličine (laserska difrakcija za analizu veličine čestica - PSD). Termičke promjene su istraživane pomoću diferencijalne skenirajuće kalorimetrije (DSC) i temperaturno programirane desorpcija (TPD). Utvrđeno je da se temperatura desorpcije vodonika snižava u prisustvu dopanta za nekoliko desetina stepeni usljed katalitičkog dejstva vanadijuma. U pogledu temperature desorpcije i prividne energije aktivacije, najbolji rezultati se očekuju za uzorak koji je mljeven 30 min, pri sadržaju aditiva of 5 mas %. Istraživanje je pokazalo da se veličina čestica značajno smanjuje čak i pri mljevenju u toku kraćih vremenskih intervala, a da se raspodjela veličine čestica mijenja od monomodalne raspodjele karakteristične za nemljeveni MgH2 do polimodalne raspodjele karakteristične za kompozite dobijene mljevenjem u toku 30 min. Primijećena desorpcija H₂ na niskoj temperaturi se može pripisati manjoj veličini čestica MgH₂. Utvrđeno je da kratka vremena mljevenja odgovaraju prividnim energijama aktivacije od 70 kJ/mol, a da dodavanje vanadijuma ne utiče značajno na temperaturu desorpcije. Ocjena o aktivnostima sprovedenim na pisanju i $\prod 2$ 3 \prod_{1} \boxtimes 5 objavljivanju naučnih radova. SAGLASNOST ZA NASTAVAK STUDIJA | | Da Može li doktorand nastaviti studije? Da, uz određene uslove lNe (Ako je prethodno dat odgovor pod "Da, uz odredjene uslove" ili "Ne" dati obrazloženje i prijedloge za poboljšanje) Napomene (Popuniti po potrebi) U Podgorici, 06.10.2023. Prof. dr Vanja Asanović dr Jasmina Grbović Novaković Sacrement Trible & Reameli MP

Prilog dokumenta sadrži:



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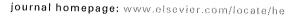
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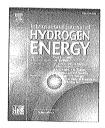
•	Objavljeni rezultati rada na izradi doktorske disertacije (za <u>drugi</u> izvjestaj mentora)				



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Hydrogen storage properties of MgH₂-Tm: Nicatalysis vs. mechanical milling

Bojana Babić ^a, Milica Prvulović ^a, Nenad Filipović ^b, Željko Mravik ^a, Zorana Sekulić ^c, Sanja Milošević Govedarović ^a, Igor Milanović ^{a,*}

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HIGHLIGHTS

- \bullet For the first time two main processes grinding and catalytic effect are separately analyzed in MgH $_2$ -Ni solid state system.
- Milling itself does not induce significant particle size reduction (for investigated milling times).
- ullet Milling process leads only to mixing of MgH $_2$ and Ni powders for milling times up to 45 min.
- Mechanical milling of MgH₂–Ni solid state system leads to better distribution of Ni particles in MgH2 bulk.
- For investigated milling times only catalytic effect of Ni is dominant.

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Hydrogen storage of MgH₂ based
system

ABSTRACT

The influence of the addition of nickel on hydrogen desorption from the MgH $_2$ –Ni composite was investigated. The composite powder was ball-milled for 15, 30 and 45 min and characterized by XRD, SEM-EDS, PSD, DSC and TPD methods. It was observed that the uniform distribution of nickel decreases hydrogen desorption temperature by more than 100 °C. A kinetic model for the hydrogen desorption process was also determined. The hydrogen desorption reaction in catalyzed samples is described by the Avrami-Erofeev model with the value of parameter n=4. The apparent activation energy of the hydrogen desorption reaction was decreased with the increase of milling time and the addition of nickel. It has been shown for the first time that two main processes (grinding and the catalytic effect) could be separately analyzed. It is concluded that for investigated short milling times, the catalytic effect of Ni is predominant.

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Introduction

Nowadays there is a great demand for renewable energy sources. Hydrogen, as one of the possible solutions has a lot of advantages in comparison to fossil fuels: oxidation in fuel cells with an absence of ${\rm CO}_2$ emission [1], supports a circular and environmentally friendly economy [2], abundance (practically unlimited quantities if produced from water) etc. The most important advantage is that the usage of hydrogen in fuel cells produces electrical current as a product and water as a byproduct which makes this process safe for the environment. In respect to the application proposes, among of three storage possibilities: gaseous, liquid and solid-state storage, only storage in solid medium meets the requirement of H2 density [2,3] (same as in the petrol tanks). Metal hydrides possess characteristics such as high volumetric density of hydrogen, high gravimetric capacity of hydrogen, good kinetics and cyclic behavior, low toxicity, low working pressure of H₂ and safety but also several drawbacks: sluggish kinetics, high desorption temperature and low thermal conductivities of pure hydrides [4].

The most investigated hydride in the last 20 years is magnesium hydride (MgH2) because of its low cost and high gravimetric capacity [4-6]. Its modification conceives better conditions for hydrogen storage [7-10]. This can be achieved by changing the microstructure of the hydride either by mechanical milling with additives [11-17], which reduces the stability of the hydride [4,11–17] or by ion irradiation [7,9]. By using the small quantities of additives (up to 10 wt%), the hydrogen storage capacity of starting hydride remains practically unchanged. As additives, metals, metal oxides and intermetallic compounds were used [4,13,18-20]. The addition of transition metals (Tm) improves hydrogen storage properties because of their simultaneous catalytic effect on sorption processes. The commonly used metals as a catalyst are nickel (Ni) [17,21-34], titanium (Ti) [11,16,20,21,28,35,36], vanadium (V) [16,21,28,37], manganese (Mn) [21], iron (Fe) [21,38], copper (Cu) [21], cobalt (Co) [21], palladium (Pd) [21] and niobium (Nb) [11,16,21,22,28,35,37,39]. Liang et al. [28] have investigated MgH_2-Tm (Ti, V, Mn, Fe, Ni) nanocomposites prepared by mechanical milling MgH $_2$ with 5 at.% of Tm within 20 h. The system $MgH_2 + 5$ at.% Ti showed the fastest desorption kinetic of hydrogen at 300 °C and 250 °C. The activation energy of this system is 71.1 kJ/mol. It is shown that $MgH_2 + 5$ at.% V can desorb hydrogen completely under vacuum within 2000 s at 300 °C and 900 s at 250 °C. Liang et al. obtained the apparent activation energy of 62 kJ/mol for the $MgH_2 + 5$ at.% V system, which is twice as less than the activation energy of pure MgH_2 (120 kJ/mol) [28]. The sorption of composite MgH $_2$ + 5 at.% V $\,$ also has been examined during 2000 cycles at 300 °C [37] by Z. Dehouche and co-workers, who concluded that the system remains stable without of reduction in kinetic rates. The lower temperature of hydrogen desorption is noticed in composite MgH_2 + 5 at.% Ti milled for 2 h. For as-received MgH_2 desorption temperature is 422 °C and for this system 370 °C. On the other hand, composite MgH_2 with 2 mol% Ni milled for 2 h at 250 °C absorbed 5.3 wt% hydrogen for only 5 min [23]. Also, next papers confirm the outstanding properties of nickel as a catalyst. Huot and co-workers investigated the presence

of nickel reduced the onset temperature of decomposition from 440.7 °C to 225.4 °C [29]. The MgH₂-Ni composite shows better kinetics when compared to the MgH2-Ni alloy because the composite has a 10 times larger specific surface area then the alloy [28]. El-Eskandarany et al. examined MgH $_2$ catalyzed with Ni nanograins, which have enormous benefits for increasing the kinetics of hydrogenation/dehydrogenation at 275 °C. The powders milled for 25 h desorbs H_2 after only 2.5 min and absorb $\rm H_2$ in 8 min, unlike MgH $_2$ which shows very slow kinetics at temperatures lower than 350 °C [30]. Gao et al. [24] investigated $MgH_2 + 7$ wt% NiV-based two dimensional layered double hydroxide and they found that the initional desorptional temperature of MgH2 was significantly reduced to 190 °C. It has been concluded that the homogeneous dispersion and unique heterostructure of Mg2Ni/Mg2NiH4 and metallic V, cooperated to provide more reaction cites and diffusion paths, enabling enhanced hydrogen storage performance of MgH₂. Hu et al. [25] investigated the system MgH₂. + 10 wt% TiMgVNi3. They found that the particle size and distribution of catalytic phases, (Ti, V)H2 and Mg2Ni are the key factor for MgH2 hydrogen desorption kinetics also. Importance of Mg₂Ni is also confermd by other authors [26,31]. Tan et al. investigated $Mg-Ni-TiS_2$ composites and found that improved hydrogen desorption kinetics is attributed ti synergetical catalalytic effect of the $\mathrm{Mg_2NiH_4}$ and $\mathrm{TiH_2}$, both form during the first absorbtion cycle [26].

In the present work, we have studied the catalytic effect of Ni particles milled with ${\rm MgH_2}$ powder and their effect on hydrogen desorption properties. The goal of our research was to investigate which of two effects is more dominant in ${\rm MgH_2}$ — Ni system: i) catalytic influence of added metal or ii) grinding effect of milling. According to our best knowledge, there are no comparative studies of these two effects on the hydrogen desorption properties.

Experimental

Pure MgH₂ (Langfang Great AP Chemicals Co, purity 98%) and system MgH₂ with 5 wt% of nickel (Johnson Matthey Alfa Products, purity 99.99%) — powders were milled for different milling times — 15, 30, and 45 min. To prevent the oxidation of the sample, the experiments were done in an inert argon atmosphere. For this purpose we have used SPEX 5100 mixer/mill (2500 RPM). The grinding vessel was made of stainless steel as well as balls. The ball to powder ratio was $\approx 16:1$.

Phase structures of the ball-milled powders were characterized by X-ray diffraction (XRD) on Rigaku Ultima IV diffractometer using a nickel filter and Cu-K α radiation ($\lambda=0.1540$ nm), in the 20 range between 10° and 90°, at operating parameters of 40 kV and 40 mA. The presented XRD measurements were made with a step of 0.02° and the accumulative time was 5 s at every point.

The distribution of particles based on their size was analyzed using Mastersizer 2000, Malvern instruments Ltd. UK which measures particle size in the range of 0.02–2000 μm using He-Ne laser ($\lambda=633$ nm). The samples were dispersed in isopropanol and after that placed in an ultrasonic bath for 5 min to avoid agglomeration.

The micrographs are obtained by Scanning Electron Microscope (SEM) JEOL JSM 6460LV and Oxford Instrument INCA-X-sight.

The thermal properties of the milled powders were measured by the DSC apparatus SETARAM DSC 131 Evo. The accurately measured samples (between 3 and 5 mg) were placed in Al measuring vessels and sealed with the lids. The samples were further subjected to a heating regime from room temperature to 530 °C, with a heating rate of 5 °C/min.

Temperature programmed desorption (TPD) was used for the analysis of desorption products during the heating. About 0.6 mg of sample was placed in a quartz cuvette. After the system is evacuated to about 1×10^{-7} mbar, the cuvette is heated at a rate of $10\,^{\circ}$ C/min from room temperature to $513\,^{\circ}$ C. The analysis of desorbed gases was carried out on a mass spectrometer Extorr 300 with five mass to charge ratio (m/z): 1 (H), 2 (H₂), 17 (OH), 18 (H₂O), and 28 (N₂ and CO).

Results and discussion

Fig. 1 shows a diffractograms of MgH $_2$ milled for 15, 30, and 45 min compared to the diffractogram of as-received (commercial) MgH $_2$. Based on the position of characteristic diffraction maxima, the presence of β — MgH $_2$ is dominant. Also, the presence of γ — MgH $_2$ phase is occurring in samples with a milling time longer than 15 min. The intensity of the

diffraction maxima is increasing with milling time, i.e. the amount of γ – MgH₂ grows, while broadening of β – MgH₂ phase diffraction maxima is evident (decrease in crystallite size). In comparison to as-received MgH₂ (which has only β – MgH₂) milled MgH₂ has broader maxima. Fig. 2 shows diffractograms of MgH₂ samples with 5 wt% Ni milled for 15, 30, and 45 min in comparison with the diffractogram of as-received (commercial) MgH₂. Three additional maxima (marked with "o" in Fig. 2 b-d) are originating from the presence of nickel [13]. By comparing the samples with (Fig. 2) and without Ni (Fig. 1), changes in phase composition during the milling process are not noticed (Table 1). This means that Ni powder does not affect the milling process. In 'Table 1 the positions of maxima for γ – MgH₂ and the nickel phase are listed.

The particle size distribution (PSD) of samples is shown in Fig. 3. As-received MgH $_2$ shows a monomodal particle size distribution with maximum of 26 μm . On the other hand, all milled MgH $_2$ samples show bimodal particle size distribution. These samples have a significantly wider range of distribution predominantly at the lower values. The decrease in particle size was noticed for a longer milling time. Table 2 shows the values of particle size range and average particle size.

Fig. 4 shows the distribution of particle sizes for asreceived MgH_2 and milled MgH_2+5 wt% Ni samples. All the MgH_2+5 wt% Ni samples have bimodal particle distribution.

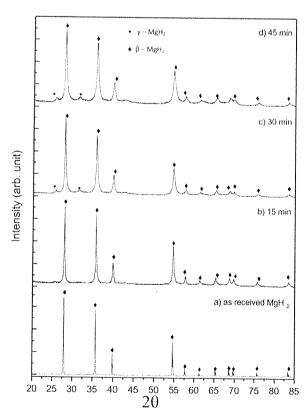


Fig. 1 — Diffractograms of as-received and milled MgH $_2$: a) as-received MgH $_2$; b) MgH $_2$ milled for 15 min; c) MgH $_2$ milled for 30 min; d) MgH $_2$ milled for 45 min.

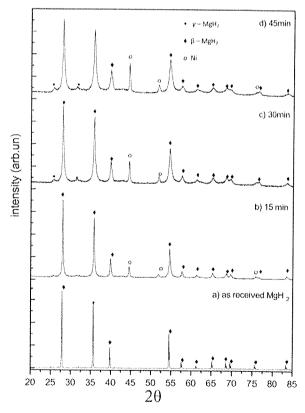


Fig. 2 – Diffractograms of as-received MgH₂ and milled MgH₂ + 5 wt% Ni: a) as-received MgH₂; b) MgH₂ + 5 wt% Ni milled for 15 min; c) MgH₂ + 5 wt% Ni milled for 30 min; d) MgH₂ + 5 wt% Ni milled for 45 min.

Please cite this article as: Babić B et al., Hydrogen storage properties of MgH_2 -Tm: Ni-catalysis vs. mechanical milling, International Journal of Hydrogen Energy, https://doi.org/10.1016/j.ijhydene.2023.04.078

Table 1 - Position of maxima for $\gamma-MgH_2$ and Ni phase on diffractograms obtained by XRD analysis of MgH_2 sample and MgH_2+5 wt% Ni sample milled for 15, 30, and 45 min.

Sample	MgH ₂ 15 min	MgH ₂ 30 min	MgH ₂ 45 min	$MgH_2 + 5$ wt% Ni 15 min	MgH ₂ + 5 wt% Ni 30 min	MgH ₂ + 5 wt% Ni 45 min
$\gamma - MgH_2$	/	54.71°(20)	27.86°(20)	/	25.71°(20)	44.53°(20)
	/	39.89°(20)	35.80°(20)	/	31.53°(20)	51.81°(20)
Ni	/	/	/	44.64°(20)	44.53°(20)	44.64°(20)
	/	/	/	51.88°(20)	51.81°(2θ)	51.92°(20)
			/	76.04°(20)	76.33°(20)	76.48°(20)

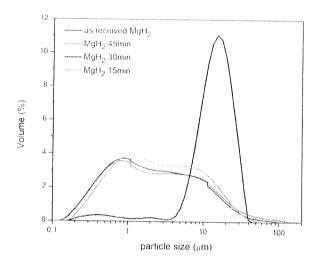


Fig. 3 - Particle size distribution (PSD) of as-received MgH $_2$ and milled for 15, 30, and 45 min.

As the milling time increases, the medium particle size remains approximately the same or minimally increased due to agglomeration. Compared to the samples without the addition of nickel, the obtained average particle sizes (see Table 2), as well as distribution widths, are slightly higher (except in the case of pure MgH $_2$ milled for 45 min which has a wider distribution range than the samples with the addition of nickel).

It is concluded that the presence of additives has little effect on the particle size distribution (see Fig. 4) Also, the distribution of particle size analysis of all MgH_2 –Ni samples

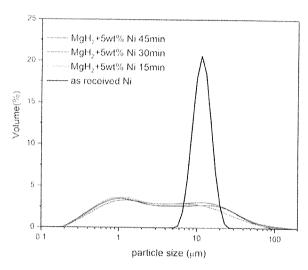


Fig. 4 – Particle size distribution (PSD) of as-received Ni, and MgH_2+5 wt% Ni samples milled for 15, 30, and 45 min.

shows that there is no significant dependence of particle size distribution and milling time (see Figs. 3 and 4).

The morphology of samples is presented by micrographs in Fig. 5. Particles of as-received MgH $_2$ powder (Fig. 5a) possess very characteristic globular MgH $_2$ particles and hexagonal Mg particles in the range between several to 25 μm . Sample MgH $_2$ + 5 wt% Ni milled for 15 min (Fig. 5b) shows the presence of irregular sponge-like particles, with dimensions from several microns to 40 μm . The increase of average particle size and

Sample	Particle size range (μm)	Average particle size (μm)
As-received MgH ₂	0.770	26
MgH ₂ 15 min	0.1-3.5	1.1
	3.559	5.5
MgH ₂ 30 min	0.1-2.1	0.9
MgH ₂ 45 min	2.1-115	5.1
	0.1-2.4	0.8
	2.4-208	4.1
MgH ₂ + 5 wt% Ni 15min	0.23.7	1.1
	3.7-141	6.4
MgH ₂ + 5 wt% Ni 30min	0.2-4.9	1.1
NE VV	4.8-187	13.2
MgH ₂ + 5 wt% Ni 45min	0.2-3.8	1.2
	3.8-100	11.7

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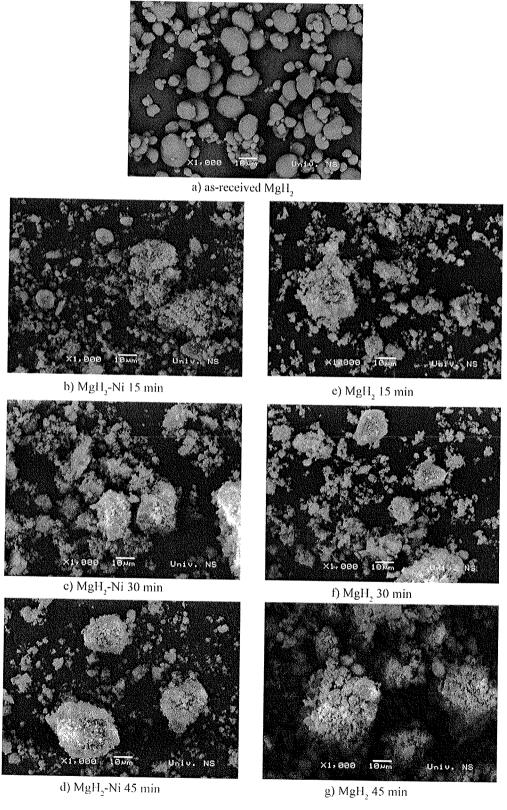


Fig. 5 - SEM micrographs of as-received MgH $_2$ (a), milled MgH $_2$ -Ni (b, c, d) and milled pure MgH $_2$ (e, f, g).

formation of larger agglomerates are visible in sample MgH $_2\,+\,$ 5 wt% Ni milled for 30 min (Fig. 5b). If the milling time increases to 45 min the predominantly irregularly shaped agglomerates with sizes between 20 and 50 μm are formed. To compare results obtained with $MgH_2 + 5$ wt% Ni system, asreceived MgH_2 was also milled for 15, 30 and 45 min. As shown in Fig. 5e, \boldsymbol{f} and \boldsymbol{g} , shape and dimensions of particles in milled MgH $_2$ are very similar in comparison with MgH $_2 \pm 5~\text{wt}$ % Ni samples. This fact indicates that nickel does not act as a milling agent in particle size reduction, and therefore has no influence on the morphology. Previous studies have demonstrated that incorporating Ni as an additive during the milling process of MgH_2 does not significantly impact the particle size of the material [40-42]. Additionally, increasing the concentration of Ni additive does not affect the particle size of MgH_2 [39].

To investigate the dispersion of Ni particles in MgH_2 all the samples with nickel are measured with SEM-EDS analysis. The EDS analysis and micrographs are shown in Fig. 6. From the SEM image of MgH_2+5 wt% Ni milled for 15 min (Fig. 6a) and its EDS profile it is obvious that round nickel particle stayed unmilled and captured in MgH_2 powder. EDS maps of nickel and magnesium prove that the dispersion of round nickel particles is very weak in magnesium hydride powder. From the SEM-EDS micrographs (Fig. 6 a and b), in the samples

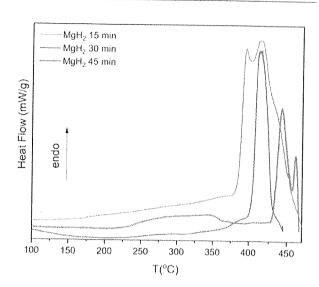


Fig. 7 – DSC curves of MgH_2 milled for 15, 30 and 45 min.

MgH $_2$ + 5 wt% Ni milled for 15 min and MgH $_2$ + 5 wt% Ni milled for 30 min, the particle of round-shaped Ni particles are clearly visible and their size correspond to the values obtained from PSD of as received Ni (around 10 μ m, Fig. 4). Finally, the

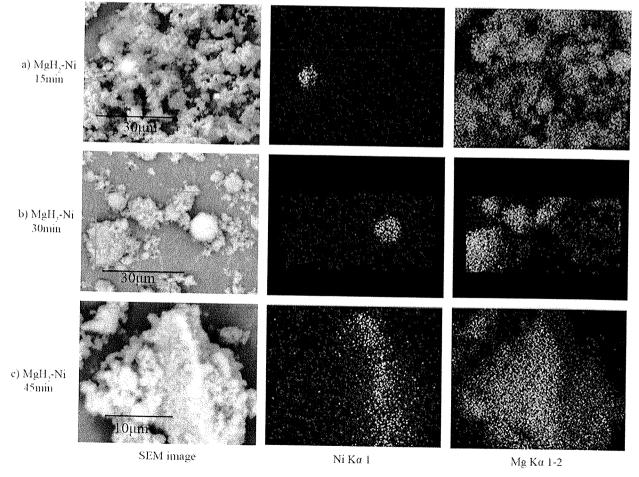


Fig. 6 – SEM-EDS micrographs of milled MgH₂-Ni composite.

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most significant changes are noticed in MgH_2 + 5 wt% Ni sample milled for 45 min (Fig. 6c). Globular nickel particles in sample milled for 45 min are reduced to very small nanometric particles which very easily penetrate in MgH_2 bulk. As a result, complete quantity of nickel powder is mixed with MgH_2 particles. The research conducted by Xie et al. [22] found that a more uniform distribution of nickel on the surface of MgH2 improves the kinetics of the dehydrogenation reaction. In the samples with weak dispersion of Ni particles, hydrogen desorption properties (DSC and TPD) are quite the same as in pure MgH₂ milled during the same period. On the other hand, a sample with a very good distribution of Ni particles (milled for 45 min) shows much better H2 desorption behavior. This can be attributed to the beneficial effect of the Ni on the hydrogen recombination reaction. The findings of this paper, which confirm the positive impact of an uniform distribution of nickel on the catalytic dehydrogenation reaction, align with previously published results [21,22,30,39,40].

The DSC curves of MgH $_2$ milled for 15, 30 and 45 min are shown in Fig. 7. The endothermic maxima are visible for all samples. Two desorption maxima at temperatures 396 °C and 416 °C are visible for MgH $_2$ milled for 15 min. The sample milled for 30 min have two maxima: shoulder at 375 °C and maximum at 414 °C. It the case of MgH $_2$ milled for 45 min, three maxima are visible: in a range of 218 °C–361 °C which belongs to hydrogen released from γ – MgH $_2$ [30], and two maxima originating from β – MgH $_2$ at 444 °C and 462 °C. With the increase in milling time, the temperature of desorption hydrogen from MgH $_2$ also increases. This behavior is a consequence of the agglomeration of MgH $_2$ particles, which is confirmed by SEM images (Figs. 5 and 6). The shorter milling time has a better influence on the properties of pure MgH $_2$ [43].

Fig. 8 shows DSC curves of MgH $_2$ with the addition of 5 wt% Ni milled for 15, 30 and 45 min. Sample MgH $_2$ + 5 wt% Ni milled for 15 min, desorbs hydrogen at 376 °C and 415 °C. For MgH $_2$ + 5 wt% Ni milled for 30 min, maxima occurs at temperatures 376 °C and 428 °C. The lowest desorption temperature (360 °C) appears in the sample milled for 45 min and the

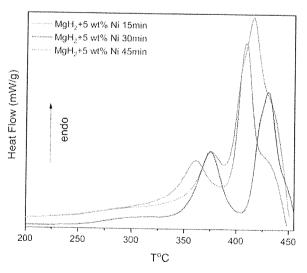


Fig. 8 – DSC curves of MgH_2+5 wt% Ni milled for 15, 30 and 45 min.

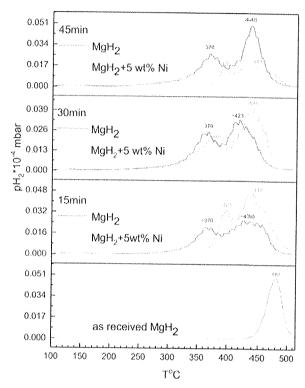
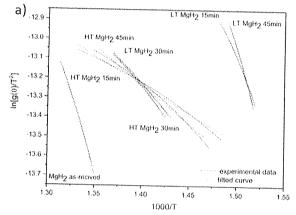


Fig. 9 — Temperature programmed desorption (TPD) profiles of as-received $\mathrm{MgH_2}$ (blue line), milled $\mathrm{MgH_2}$ (red line), and milled $\mathrm{MgH_2} + 5$ wt% Ni (black line). (For interpretation of the references to color in this figure legend, the reader is referred to the Web version of this article.)

second maximum appears at 410 °C. Shoulder in the range of 275–325 °C, analogue to the sample MgH₂ milled for 45min, also originates from γ – MgH₂ phase. In all milled samples, with and without Ni, two desorption maxima are present. These maxima are a direct consequence of bimodal particle size distribution (Figs. 3 and 4). In the case of the addition of Ni, a catalytic effect is the most pronounced, especially in the sample MgH₂ + 5 wt% Ni milled for 45 min due to excellent distribution of Ni in MgH₂, confirmed by SED-EDS (Fig. 6 c).

In Fig. 9 the TPD profiles of as-received MgH2, milled MgH2, and $MgH_2 + 5$ wt% Ni are shown. TPD analysis of as-received \mbox{MgH}_2 (Fig. 9, blue line) shows that hydrogen desorption begins at 441 °C while the desorption maximum is present at 480 °C. The presence of only one desorption maximum is following the literature data [10,43,44]. As shown in Fig. 9 (red line), hydrogen is released at lower temperatures in the case of the milled samples. The low-temperature (LT) maxima for the samples milled for 15 and 45 min are at 400 °C and 392 °C, while for the sample milled for 30 min, the maximum is at 366 °C. The high-temperature (HT) maximum for all the samples is at 440 °C, but the maximum narrows with the increase of milling time, i.e. hydrogen is released in a shorter time and temperature interval. In comparison with the results of TPD analysis and DSC analysis, we can conclude that the maximum at lower temperature belongs to the hydrogen desorbed from smaller particles, obtained after milling, while

Sample	Peak	0	yrami — Erofeev model for $n = 3$ E_a for $n = 4$ (kJ/mol)	E_a for $n = 3$ (kJ/mol
As-received MgH ₂	/	0.20-0.80		
MgH ₂ 15min	LT	0.200.80	90 ± 2	124 ± 2
MgH ₂ 15min	HT		92 ± 2	126 ± 3
MgH ₂ 30min	LT	0.12-0.85	32.6 ± 0.4	47.6 ± 0.5
MgH ₂ 30min		0.25-0.80	44.6 ± 0.4	63.4 ± 0.5
MgH ₂ 45min	HT	0.25-0.80	47.1 ± 0.6	66.8 ± 0.8
0 -	LT	0.200.80	133 ± 3	181 ± 4
MgH ₂ 45min	HT	0.13-0.88	24.1 ± 0.2	36.0 ± 0.3
MgH ₂ + 5 wt% Ni 15min	LT	0.15-0.85	26.6 ± 0.3	
MgH ₂ + 5 wt% Ni 15min	HT	0.20-0.80	35.9 ± 0.4	39.0 ± 0.4
MgH ₂ + 5 wt% Ni 30min	LT	0.100.60	45.1 ± 0.2	51.9 ± 0.6
MgH ₂ + 5 wt% Ni 30min	HT	0.260.74		64.0 ± 0.2
MgH ₂ + 5 wt% Ni 45min	LT	0.20-0.70	43.1 ± 0.5	61.3 ± 0.7
MgH ₂ + 5 wt% Ni 45min	HT		27.7 ± 0.2	40.4 ± 0.3
	111	0.200.70	36.7 ± 0.4	52.3 ± 0.5



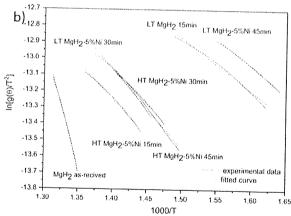


Fig. 10 – The plot of $\ln [g(\theta)/T^2]$ function vs. 1000/T for a) LT and HT maxima of MgII₂. Experimental data and fit with the best linearity obtained for nucleation model $g(\theta) = [-\ln (1-\theta)]^{(1/n)}$, for n=3 b) LT and HT maxima of MgH₂ + 5 wt% Ni. Experimental data and fit with the best linearity obtained for nucleation model $g(\theta) = [-\ln (1-\theta)]^{(1/n)}$, for n=4.

the more intense maximum is at higher temperature and it originate from presence of hydrogen desorbed from $\beta-MgH_2$ and agglomerates [43].

Desorption temperatures for milled MgH $_2$ + 5 wt% Ni (black line) are slightly lower regarding to the desorption temperatures for the milled pure MgH $_2$, and as much as 110–40 °C lower than the hydrogen desorption temperature for the asreceived MgH $_2$. The first maximum for all samples is evident at 370 °C, approximately. The maxima of the samples milled for 15, 30, and 45 min are at 429 °C, 423 °C, and 441 °C. The second maximum becomes narrower with the increase of milling time, i.e. the hydrogen is released over a shorter period of time in a linear temperature range which is a consequence of the catalytic effect of nickel.

Kinetic models for the hydrogen desorption process were investigated. The activation energy values are obtained (Table 3) by fitting experimental data to the kinetics models. The samples, in which unequivocal observation of the desorption maximum was possible, were examined: as-received MgH₂, MgH₂ milled for 30 min and MgH₂ + 5 wt% Ni milled for 30 and 45 min. The kinetic model Avrami-Erofeev showed the best linearity (Fig. 10) with n=3 and n=4 which is described by a function:

$$g(\theta) = [-\ln(1-\theta)]1/n$$

where n is reaction order and represents the sum of λ and β . λ is the dimensionality factor and it describes the dimensional growth of nucleation nuclei. It has values 3, 2 and 1. When $\lambda=1$, we have one-dimensional (1D) growth of the nucleus of the formed phase, $\lambda=2$ -2D growth, and when $\lambda=3$ there is three-dimensional (3D) growth of magnesium nucleation nuclei. Factor β is constant and describes the character of the process. It adopt values of 0 and 1 depending on whether the number of growing nuclei is constant or it changes [44]. It is assumed that hydrogen desorption reaction is a 4th order reaction. The growth of magnesium nuclei considers to be three-dimensional (3D). It is observed extensive difference in values of apparent activation energy for low-temperature (LT) and high-temperature (HT) maxima for MgH₂ milled for 30 and 45 min is observed (Table 3, Fig. 10).

The value of apparent activation energy (E_a) of MgH₂ milled for 30 min is twice as less than the value of the as-received MgH₂, which can be explained with by the reduction of the particle size. In MgH₂ + 5 wt% Ni sample with the same milling

time, it has been noticed that values of Ea are lower by several kJ/mol due to the catalytic effect of Ni. The sample with the addition of nickel milled for 45 min has the lowest value of $E_a = 27.7 \; kJ/mol \; for \; the \; LT \; maximum, \; and \; 36.7 \; kJ/mol \; for \; the \;$ HT maximum. Those values are in correlation with the assumption that with the longer milling time the dispersion of nickel is better in MgH_2 bulk, which has catalytic effect on the hydrogen desorption reaction [16,22,23]. The catalytic effect of Ni on H_2 desorption from MgH_2 by lowering E_a was proved by Hanada et al. [21] who found that by incorporating the 2 mol% of Ni and grinding for 15 min, the activation energy for the dehydrogenation reaction was 94 kJ/mol. Similarly, Xie et al. [39] discovered that by adding 10 wt% Ni and grinding for 2 h, the activation energy is 118 kJ/mol while the addition of 25 wt % Ni, reduced the activation energy to 82 kJ/mol. On the other hand, Cova et al. [45] were able to decrease the activation energy to 117 kJ/mol by grinding MgH_2 with 1 mol% Ni for 10 h. Yang et al. have obtained a similar value of E_a 83 kJ/min for the sample with the addition of 5 wt% Ni milled for 3 h [42]. The decrease in value of Ea is a direct consequence of the uniform dispersion of nickel particles in MgH2 (Fig. 6 SEM-EDS) with the increase of milling time. The catalytic effect of Ni can be explained through effects of physical interface between metal catalyst and investigated metal-hydride (MgH₂). Ouyang et al. [46] assert that reduction of desorption temperature is a direct consequence of change of interface energy along high interface density. In sample $MgH_2 + 5$ wt% Ni milled for 45 min, Ni is highly distributed in the MgH2 matrix, reaching high interface density. In the interface, extra energy is stored, and it can reduce the energy barrier for formation of new phases. Metal catalysts with good, homogeneous dispersion in matrix, provide more reaction sites and diffusion channels and desorption occurs over edge sites [24,25]. After dehydrogenation of the sample, formation of new phase Mg₂Ni was proved [24-26] which have a key role in accelerating of further sorption reaction. Finally, Mg₂Ni phase would act as a "hydrogen pump" in further absorption/desorption cycles [32,33] by destabilizing Mg–H bond of MgH2 and facilitate hydrogen dissociation due to high affinity toward hydrogen [31,34].

Conclusions

Two main processes, grinding and catalytic effect, are separately analyzed in MgH2-Ni solid-state system. By applying short milling intervals, MgH₂–Ni system has shown adequate behavior as a medium for hydrogen storage. The SEM-EDS measurements confirmed uniform distribution of Ni particles in MgH2 powder for milling interval of 45 min, but morphological and microstructural properties of MgH2-Ni system are not significantly changed. As a consequence of better Ni particle distribution, in comparison with pure MgH₂, lower apparent activation energy (Ea) and H2 desorption temperature are noticed. The best explanation of hydrogen desorption reaction shows Avrami-Erofeev model, for parameter n = 4. Based on SEM, TPD, and kinetic model fitting, two very important consequences are obvious: the influence of mechanochemical grinding of materials is minimized, while the dependence of the nickel powder distribution in MgH_2 bulk on the milling time is dominant. By using short

milling times, grinding effect was minimized and the only predominant effect is the catalytic effect of Ni on the $\rm H_2$ desorption from MgH₂.

Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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The Catalytic Effect of Vanadium on Sorption Properties of MgH₂-Based Nanocomposites Obtained Using Low Milling Time

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Abstract: The effects of catalysis using vanadium as an additive (2 and 5 wt.%) in a high-energy ball mill on composite desorption properties were examined. The influence of microstructure on the dehydration temperature and hydrogen desorption kinetics was monitored. Morphological and microstructural studies of the synthesized sample were performed by X-ray diffraction (XRD), laser particle size distribution (PSD), and scanning electron microscopy (SEM) methods, while differential scanning calorimetry (DSC) determined thermal properties. To further access amorph species in the milling blend, the absorption spectra were obtained by FTIR-ATR analysis (Fourier transform infrared spectroscopy attenuated total reflection). The results show lower apparent activation energy (Eapp) and H₂ desorption temperature are obtained for milling bland with 5 wt.% added vanadium. The best explanation of hydrogen desorption reaction shows the Avrami-Erofeev model for parameter n = 4. Since the obtained value of apparent activation energy is close to the Mg-H bond-breaking energy, one can conclude that breaking this bond would be the rate-limiting step of the process.

Keywords: hydrogen storage; magnesium hydride; transition metals; additives; mechanochemistry

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1. Introduction

Hydrogen as an energy vector represents great potential due to its high gravimetric density and low mass, as well as the fact that combustion does not emit harmful chemical byproducts. Hydrogen has the highest energy density per unit mass compared to any other fuel but a rather low energy density per unit volume. Further, hydrogen storage is a key technology for developing a hydrogen and fuel cell-based economy [1]. Metal hydrides as alternative hydrogen carriers have various performance parameters such as operating temperature, sorption kinetics, activation conditions, cyclic options, and equilibrium hydrogen pressure. These parameters can be improved or adjusted to meet the technical requirements of different applications [2]. Hydrogen in metal hydrides is chemically bonded, usually much stronger than the physical bonding present during hydrogen adsorption. Consequently, more energy is needed to release chemically bound hydrogen [3]. On the other hand, a stronger bond between hydrogen and metal hydride allows the storage of higher hydrogen densities even under ambient conditions [4]. Magnesium hydride is recognized as an excellent material for solid-state hydrogen storage due to its high

gravimetric hydrogen capacity, good reversibility, and low cost. However, its practical application is limited by high thermodynamic stability and slow sorption kinetics [5]. To overcome the mentioned shortcomings, most of the research on magnesium hydride-based materials focuses on improving volumetric and gravimetric capacities, hydrogen absorption/desorption kinetics, and thermodynamics [1-5]. Mechanochemical modifications of the crystal structure of magnesium hydride and doping with the transition metals is a possible path for improving sorption properties. Doping with transition metals and their alloys is generally considered the simplest method to accelerate the sorption kinetics of MgH₂. Most of the activities done in this field to the present day have been devoted to mechanochemical modifications using long milling times [1-16]. Sun et al. [4] compared the influence of transition metals in combination with carbon materials on the storage properties of hydrogen in MgH2. The desorption properties of the tested systems can be ranked as follows: Mg-Ti > Mg-Nb > Mg-Ni > Mg-V > Mg-Co > Mg-Mo. These composites can release hydrogen at temperatures below 225 °C, significantly lower than pure MgH₂. Liang et al. [6] investigated the influence of 3d transition metals Ti, V, Mn, Fe, and Ni as additives on the sorption properties of MgH_2 , where powder nanocomposites were synthesized by a 20 h milling process. Desorption was fastest in the system MgH₂-V, then MgH_2 -Ti, MgH_2 -Fe, MgH_2 -Ni, and MgH_2 -Mn at lower temperatures. On the other hand, the fastest absorption kinetics were determined for Mg-Ti, then Mg-V, Mg-Fe, Mg-Mn, and finally Mg-Ni. Of the investigated transition metals, V and Ti showed a better catalytic effect than Ni during hydrogen absorption and desorption. Composites with V or Ti as an additive showed fast desorption kinetics above 250 °C and absorption kinetics at temperatures below 30 $^{\circ}$ C. When examining the desorption properties of an MgH₂-V system prepared by ball milling, Liang et al. [7] concluded that MgH_2-5 at.% V can desorb hydrogen at 200 $^{\circ}\text{C}$ and reabsorb hydrogen faster even at room temperature. It was found that the apparent activation energy of hydrogen desorption was reduced to 62 kJ/mol. Gasan et al. [8] investigated the influence of 5 wt.% of additives (V, Nb, and Ti) on the desorption temperature of hydrogen in MgH₂. X-ray powder diffraction (XRD) results showed that adding vanadium powder significantly affected the transformation of Mg to MgO or hydride because the amount of MgO in the MgH2-V system was higher than in other systems. Scanning electron microscopy also showed a significant reduction in the particle size of the powder. The results obtained by differential scanning calorimetry showed that the addition of 5 wt.% additive reduces the desorption temperature of hydrogen in MgH₂ by about 40-50 °C. Lu et al. [9] investigated the catalytic effect of two-dimensional (2D) vanadium nanoplates (VNS) on MgH2 for hydrogen storage purposes. It was found that the composite $MgH_2 + 7$ wt.% VNS begins to release hydrogen at 187.2 °C, or at a temperature 152 °C lower than MgH $_2$ without additives. Within 10 min at 300 °C, 6.3 wt.% of hydrogen was released from MgH₂ + 7 wt.% of VNS composites. Additionally, a completely dehydrated sample can absorb hydrogen at room temperature under a hydrogen pressure of 3.2 MPa. Hanada et al. [10] investigated the catalytic effect of nanoparticles on 3d transition metals on hydrogen desorption in MgH2 prepared by ball milling. All MgH2 composites prepared by adding a small amount of Fe, Co, Ni, and Cu metal nanoparticles and ball milling for 2h show much better hydrogen desorption than pure MgH_2 . The best properties were observed for an MgH₂-based composite doped with 2 mol.% Ni nanoparticles and prepared by short-term (15 min) low-intensity ball milling (200 rpm). A large amount of hydrogen (~6.5 wt.%) was found to be desorbed in the temperature range from 150 $^{\circ}\text{C}$ to 250 °C by heating at a rate of 5 °C/min under a flow of He gas, practically without partial hydrogen pressure. According to DFT calculations done by Paskaš Mamula et al. [11], adding Fe, Ni, and Co will improve desorption kinetics due to the higher stability of Tm-H bonds. The final remark of numerous scientific papers on this topic is that transition metals have great potential in the choice of dopants from the aspect of improving sorption kinetics and reducing the activation energy of hydrogen desorption. On the other hand, most of the studies presented so far used similar high-energy mills and concerned milling at long times, from 1 to 25 h [1-10,12-17]. Further, as observed by Czujko et al. [18] there is not

much difference in sorption kinetics of the mechanically modified MgH_2 due to changes in the particle and crystallite size of the powder particles. Therefore, it is difficult to determine a parameter that influences kinetics.

In this paper, we have examined the structural transformations that occur in dopped MgH_2 systems with different concentrations of vanadium at low milling times ranging from 15 to 45 min and correlated to the thermal behavior of the samples and kinetics.

2. Materials and Methods

Magnesium hydride (Langfang GreatAP Chemicals Co., Langfang, China, purity 98%) with the addition of vanadium (Merck, Rahway, NJ, USA, purity 99.99%) in different weight percentages (2 and 5 wt.%) was synthesized at different time intervals (15, 30, and 45 min) in an inert argon atmosphere to prevent oxidation of the sample, using BPR (Ball to Powder Ratio) $\approx 10:1$. Mechanochemical synthesis was done in the SPEX Sample Mixer/Mill 5100 mill using stainless steel vial and balls, stainless steel jars, vials 1.2", 1 gr balls, with a total of 100 mg sample amount [19]. The intensity of ball milling was 2500 rpm. The composition and parameters of milling are given in Table 1.

Table 1. The lis	of prepared	samples and	milling conditions.
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Composition	wt.% V	Milling Time [min]		ame
Mall	2	15 30 45	2V	2V15 2V30 2V45
	5	15 30 34	5V	5V15 5V30 5V45

Structural characterization of material was performed using X-ray diffraction analysis (XRD) on a Rigaku Ultima IV diffractometer using a nickel filter and Cu K α radiation (while wavelength was 0.1540 nm), in the 20 range between 20 and 90°, at operating parameters of 40 kV and 40 mA, a step of 0.02°, the accumulative time of 5 s in every point and a silicon strip detector counter. The particle size distribution was analyzed using Mastersizer 2000, (Malvern Instruments Ltd., Malvern, UK) according to the standard procedure explained by Milanović et al. [20]. The desorption properties of the milled samples were measured by DSC apparatus SETARAM DSC131 using a heating rate of 10 °C/min, and temperature-programmed desorption (TPD) using homemade apparatus equipped with a mass spectrometer Extorr 300 at the same heating rate [21]. Iso-conventional kinetic methods and the Avrami-Erofeev kinetic model are described elsewhere [21].

3. Results

3.1. Microstructural and Morphological Characterization

As shown in Figure 1, sharp diffraction maxima at positions $2\theta = 27.63^{\circ}$ (110), 35.62° (101), 39.48° (200), 54.21° (211), are characteristic of β -MgH₂ with tetragonal structure, space group P₄₂/mnm (No. 136) [22]. Low-intensity diffraction maxima at $2\theta = 32.18^{\circ}$ (100) and 36.63° (101) originating from metallic Mg as expected given the initial composition of the sample (98% purity). There are no peaks corresponding to the crystalline phases of Mg(OH)₂ and MgO.

Figure 2 shows diffractograms of all samples obtained using different milling times. The tetragonal β -MgH₂ is the dominant phase, although a small amount of γ -MgH₂ phase is present in samples even after 15 min of milling. The intensity of γ -MgH₂ diffraction maxima increases with the increase of milling time since the amount of γ -MgH₂ increases. The broadening of β -MgH₂ phase diffraction maxima is visible, too, indicating a decrease in crystallite size. A similar was found by Varin et al. [23]. They have shown a spread of diffraction maxima in β -MgH₂ that increases with increasing milling time. The authors

associated this phenomenon with a decrease in crystallite size, which may be accompanied by the appearance of lattice micro-stress. Mixing with additives also introduces stress into the lattice, leading to peak broadening [12]. We expect similar behavior of samples milled with vanadium (see Table 2).

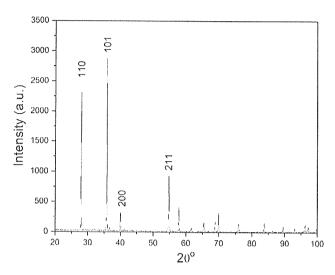


Figure 1. XRD pattern of as-received MgH₂.

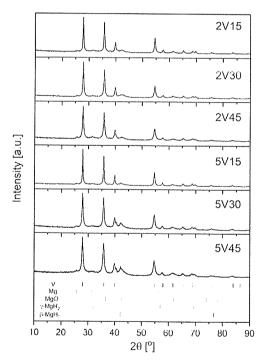
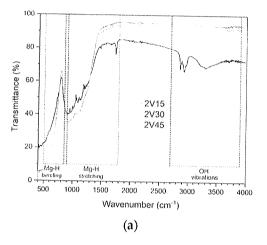


Figure 2. Diffractograms of milled MgH_2 -V composites obtained with different quantities of Vanadium (2 and 5 wt.%) and milled for 15–45 min.

Table 2. Crystallite size dependence on milling time and chemical composition.

V Content (wt.%)/Milling Time (s)	15	30	45	
0	20	39	30	
2	39	35	30	
5	46	30	25	

FTIR-ATR spectra for the samples milled with 2 and 5 wt.% of vanadium. are given in Figure 3a,b, respectively. Three regions are clearly distinguished: the first (500–800 cm $^{-1}$) corresponds to Mg-H bending vibrations, the second (900–1300 cm $^{-1}$) corresponds to Mg-H stretching vibrations [24], and for the 2V15 sample, and the third region (2500–3900 cm $^{-1}$) corresponds to the observed OH group vibrations. For all three 5V samples, OH vibrations at 3670 cm $^{-1}$ are observed. The largest changes are observed in the region 900 cm $^{-1}$ FTIR-ATR spectra of MgH₂ samples milled with 2 wt.% V (a) and 5 wt.% V (b) samples.



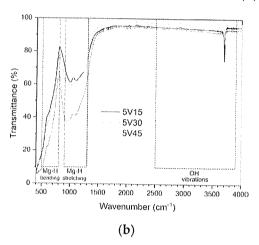
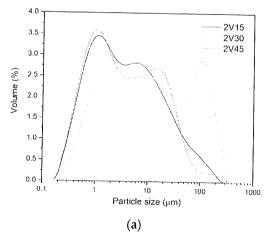


Figure 3. FTIR-ATR spectra of samples of MgH_2 samples milled with 2 wt.% V (a) and 5 wt.% V (b) samples.

Figure 4 shows the comparative distribution of particle sizes for all samples. As shown in Figure 4a, for all three milled blends with 2 wt.% of vanadium, about 30% of the particles have an average particle size of about 1 μm . Sample 2V15 has about 70% of particles with an average size of about 10 μm . As milling time increases, the average particle sizes increase due to agglomeration, and distribution becomes polymodal. This is followed by the specific surface area decrease of almost 50% for 2V and 5V samples. In Figure 4b the particle size distribution of samples milled with 5 wt.% of vanadium for different milling times: 15, 30, and 45 min (5V15, 5V30, and 5V45). The 5V15 sample has a particle size distribution in the range of 0.2–91.2 μm (about 75% of the sample is in the range of 0.2–10 μm , with an average value of 2.5 μm , while about 25% of the sample in the range of 10–91.2 μm , with the medium particle size of 39.3 μm).



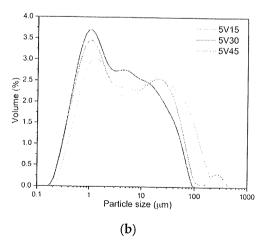
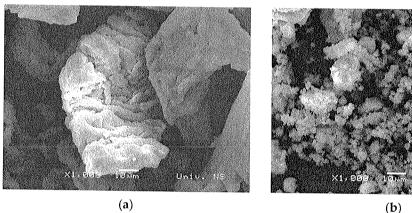


Figure 4. Particle size distribution of MgH_2 samples milled with 2 wt.% V (a) and 5 wt.% V (b) samples.

The 5V30 sample is characterized by the widest distribution of particle sizes, polymodally distributed, where 65% of the sample consists of particles of 0.2–10 μ m, with an average particle size of 2.3 μm . In the range of 10–100 μm , there is 30% of the sample, with an average particle size of 39.3 μ m. The residue is outside this range, i.e., 100–416 μ m, with an average particle size of 229 μm . The 5V45 sample has a similar polymodal particle size distribution as the 5V30 sample. Here, in the range of 0.2–10 μm , almost 60% of the sample is present, with an average particle size of about 2.62 μ m; in the range of 10–100 μ m there is about 37% of the sample, with an average particle size of 39.3 μm and the rest of the 5V45 sample powder consists of particles above 100 μ m (from 100–316 μ m) with an average particle size of 140 μm . Mechanical milling by adding 5 wt.% of the catalyst changes the shape of the distribution. However, as with the milled commercial material, the distribution is bimodal, except for the 5V30 sample, where the distribution is polymodal.

The images obtained by SEM analysis (Figure 5) correlate with the particle size distribution analysis results. Commercial powder particles are irregular in shape with a layered structure, rough on the surface with a size above 100 μm , while powder particles MgH₂ mechanically milled for 10 h are spongy in structure, with different sizes ranging from below 1 µm to 50 µm.



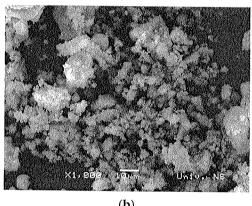


Figure 5. SEM micrographs of (a) commercial MgH2 powder and (b) MgH2 powder milled for 10 h.

SEM-EDS micrographs of composites MgH₂-V show that vanadium layer particles are captured in MgH₂ powder (Figure 6). EDS maps of vanadium and magnesium prove that the dispersion of vanadium particles is very weak in magnesium hydride powder, but the size of vanadium particles increases with the increase of milling time. As shown by Bassetti et al. [25], the microstructure and morphology of MgH₂-Fe nanocomposites can be changed by turning the ball milling energy and catalyst concentration, thus affecting the kinetic features of the hydride decomposition. The microstructure-sorption properties interplay was and still is the subject of extensive research [23,26,27]. Czujko et al. first demonstrated that microstructure changes occur in the first few minutes of mechanical activation [18].

3.2. Thermal and Kinetic Characterization of Materials

The TPD profiles of recombined hydrogen (H₂), H⁺, OH⁻, and H₂O from 2V15 (a) and $5\mathrm{V}15$ (b) samples have been shown in Figure 7. Multiple peaks at different temperatures suggest the existence of differently bonded hydrogen atoms in the samples [22]. If a low quantity of catalyst is added, there is a pronounced recombination of hydrogen and oxygen to form $\mathrm{H}_2\mathrm{O}$, but also some OH^- ions are present too, possibly from the amorphous Mg(OH)₂ phase [28], while in the 5V15 sample low-temperature peak originates from the recombination of H⁺ to H₂ [29]. The existence of a low-temperature H₂ peak is due to smaller hydride particles.

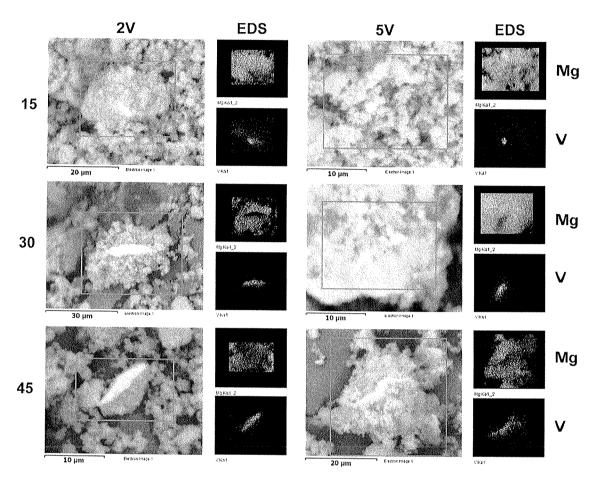


Figure 6. SEM micrographs and corresponding EDS Mg and V spectra of MgH_2 samples milled with 2 wt.% V (2V) and 5 wt.% V (5V) samples.

The DSC curve of commercial powder MgH₂ shows the endothermic desorption maximum of hydrogen at 454 °C (high temperature, HT), a value comparable to the literature [30]. As indicated earlier, a sharp symmetric HT maximum originates from desorption from rutile-structure (β) MgH₂. The maximum of very low intensity (intermediate temperature, IT) is observed at about 350 °C, which is also expected [29]. IT peak is a consequence of surface-bound OH groups. Suppose the sample is exposed to the atmosphere and oxidation for a long time, a third, low temperature (LT) maximum [24,25] may occur, which originates from OH groups and water. It is observed that the hydrogen release temperature increases with increasing milling time, meaning that shorter milling times have an improving effect on the desorption properties of MgH₂ [18]. Figure 8a shows the thermograms obtained by DSC for 2V15, 2V30, and 2V45 samples. The endothermic desorption process in this composite significantly differs from the desorption from 5V samples. There is no desorption at low temperatures. Samples 2V15 and 2V30 composites are similar to pure milled hydride, with a wide maximum occurring at medium temperatures and an onset temperature of about 250 °C. For composites milled for 15 and 30 min, the maximum is shifted to temperatures above 454 °C. At temperatures of 450 °C and 460 °C, hydrogen is released from Mg(OH)2 due to the oxidation of MgH2 with oxygen from the air [31,32]. Figure 8b shows the thermograms obtained by DSC for 5V15, 5V30, and 5V45 samples. All three samples show a significantly different desorption profile than the commercial sample. The absence of desorption from medium temperatures is visible, but a pronounced LT peak appears at approximately 110 °C.

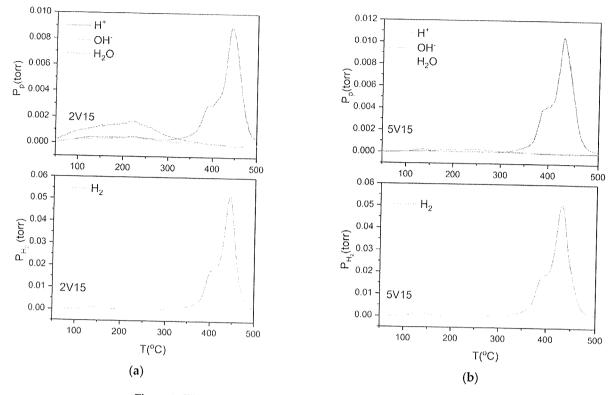


Figure 7. TPD profiles of MgH $_2$ samples milled with 2 wt.% V (a) and 5 wt.% V (b) samples.

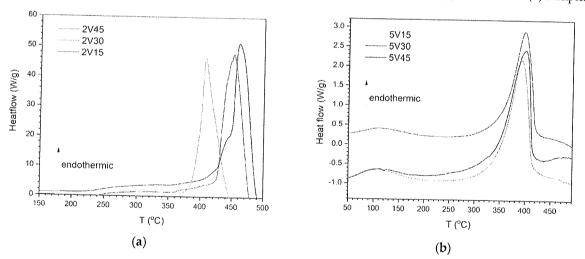


Figure 8. DSC curves MgH_2 samples milled with 2 wt.% V (a) and 5 wt.% V (b) samples.

For sample 5V15, the HT maximum occurs at 392 °C and corresponds to the release of hydrogen from $\beta-MgH_2$ (Table 3). The shift of the maximum by 62 °C is attributed to the reduction of the hydride particle size caused by mechanical milling. Similar behavior is shown by the other two composites milled for a longer time. The observed asymmetry of the DSC peaks could be explained by different PSDs and the presence of the gamma phase, as explained by Varin et al. [33].

Table 3. Positions of low temperature (LT), intermediate temperature (IT), high temperature (HT), and very high temperature (VHT). DSC maxima and corresponding apparent activation energies (Eapp). Estimated errors are given in parentheses.

Sample	LT (°C)	Eapp (kJ/mol)	IT (°C)	Eapp (kJ/mol)	HT (°C)	Eapp (kJ/mol)	VHT (°C)	Eapp (kJ/mol)
5V15	111.4(9)	4.91(7)	371.4(7)	27.7(3)	396.12(6)	00/15		
5V30	114.7(4)	5.21(7)	368.1(6)	` '	· · · /	90(1)	469.9(6)	60.3(2)
5V45	115.0(6)	· · ·	` '	25.9(3)	392.01(4)	78(1)	452.4(7)	61.5(7)
0130	115.0(6) 3.38(6)	3.38(0)	371.5(6)	32.3(3)	398.03(4)	82(1)	-	
2V15	420(2)	59.5(4)	437.9(2)	224(2)	463.8(2)			
2V30	- '	~ (~)	436.82(8)	` '	(' /	108.9(7)	-	-
2V45			430.02(0)	250(2)	451.22(7)	96.9(5)	-	_
4 V 30	-	-	-	-	408.6(1)	106.7(7)	428.7(3)	158(1)

Section 3.1 shows no significant changes in microstructural morphology upon short-term milling since similar microstructure and morphology were obtained for pure MgH_2 [31]. This leads us to the conclusion that the addition of vanadium affects the thermal desorption of the material.

To investigate the desorption process in detail, different models of solid-state kinetics were used as implemented in the code developed in our group. The rate-limiting step of the desorption reaction was determined using the iso-conversional kinetic method due to better accuracy of obtained apparent activation energies [21,34]. As shown in Table 3, showing the received MgH₂ and milled one, for the same milling time [31], a decrease in apparent activation energies has been observed. It is obvious that the sorption kinetics is affected by material preparation because the reactivity of magnesium with hydrogen is strongly modified by changes in several surface parameters that govern the chemisorption, the dissociation of molecular hydrogen, and hydride nucleation [35,36]. Cui et al. [37] explained that desorption is affected significantly by the gas-solid interface. The first work by Isler [38] proposed that the reactivity of magnesium is determined by the free magnesium surface, while Vigeholm [39] indicates that surface nucleation and growth with a pressure-dependent concentration of nuclei is the mechanism of desorption. Therefore, the thermal decomposition of MgH2 is a heterogeneous reaction. If there is an additive in milling bland, the sorption kinetics is also affected by the reaction at the Mg-Tm metal surface [11], but also the dispersion of Tm must be considered when defining a mechanism of desorption [12]. As shown in Table 3, adding 5 wt.% of vanadium leads to a significant decrease in apparent activation energies and temperature, 78 kJ/mol and 392 °C. An explanation of the change of mechanism is given. This value of apparent activation energy is close to the Mg-H bond-breaking energy suggesting that the breaking of this bond would be the rate-limiting step of the process [40]. The kinetic analysis done by Perejon et al. [40]. on pure MgH_2 shows that the reaction of desorption follows the first-order kinetics, equivalent to an Avrami-Erofeev kinetic model with a corresponding coefficient equal to 3, suggesting that the mechanism of tridimensional growth of nuclei previously formed (A3) if desorption is done under pressure. Similar is obtained by other authors [4-10,12-16]. The additive change mechanism of desorption to Avrami Erfeev with parameter 4 (A4) is shown in Figure 9. Random nucleation is observed in all systems where defects are introduced [34].

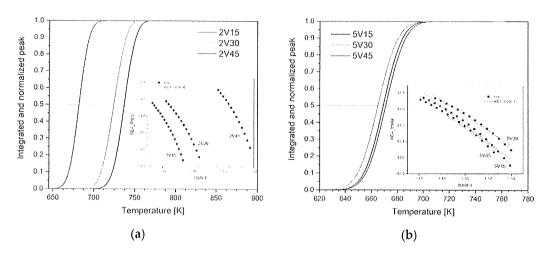


Figure 9. Temperature evolution of the reacted fraction (q) corresponding to MgH₂-V decomposition, obtained by integration of HT-H₂ peaks for mailing blends with 2 and 5 wt.% of vanadium and MgH₂. Inserted figure: From ln g(θ) = f(1/T), the best fit of experimental data is obtained for nucleation. (a) sample with 2 wt.% of V, (b) sample with 5 wt.% of V.

4. Conclusions

Using mechanochemical milling as a green synthesis method in an inert argon atmosphere, a magnesium hydride-vanadium composite was synthesized with a ball-to-powder mass ratio of 10:1, but different milling times from 15 to 45 min. As an additive, vanadium was added in 2 wt.% and 5 wt.%. The microstructure and morphology of the samples were examined and correlated with desorption properties monitored. The microstructure was monitored by X-ray diffraction analysis and infrared spectroscopy with Fourier transform, while morphology was examined by particle size distribution and scanning electron microscopy (SEM). The thermal behavior of milling blends was followed by TPD and DSC measurements. It was noticed that the presence of a dopant lowers the desorption temperature of hydrogen by several tens of degrees due to the catalytic action of vanadium. The best performance according to desorption temperature and apparent activation energy is expected for the 5V30 sample. Particle size distribution showed that even short milling times significantly reduce the particle size, which changes from a monomodal for as-received MgH₂ to a polymodal distribution for milling blends milled for 30 min. As this distribution follows the particle size distribution of pure, milled MgH2, we can assume that the decrease in desorption temperature is due to the added catalyst and its distribution in the bulk of the material. It has also been observed that, depending on the catalyst concentration, the temperature maximum shifts to the left or right of the value characteristic of pure hydride. TPD and FTIR measurements demonstrate the existence of OH- ions and H₂O molecules. Those species give rise to intermediate and low-temperature desorption. Low-temperature desorption of H₂ is noticed and can be ascribed to a lower particle size of MgH₂. It is shown that short milling times correspond to apparent activation energies of 70 kJ/mol, comparable to results obtained using longer milling times. Also, adding V using high-energy ball milling does not drastically influence the desorption temperature. This implies that it is better to use shorter milling times.

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